A Computational Study of the Decomposition of Carbon Tetrafluoride in Wet Argon under Electron Beam Irradiation

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In this study, a computational method of the kinetic model of carbon tetrafluoride (CF₄) in wet argon gas under electron beam irradiation was developed. Using this method, the mechanism of decomposition and the optimum concentration of H_2O during decomposition of CF₄ was determined. It was found that 99% of 1000 ppm of CF₄ of in atmospheric-pressure argon gas decomposed at an input energy density of 1 J/cm³.

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1. Introduction

The removal of per-fluorocompounds (PFCs), such as CF_4 and C_2F_6 , is important for the abatement of greenhouse gases from a semiconductor facility. Non-thermal plasma technology has been applied to the decomposition of PFCs [1]. In non-thermal plasmas, electron impact reactions and ion reactions with PFCs are the dominant decomposition processes, because PFCs are inherently inert to radicals.

A non-thermal plasma is usually generated by a discharge. In non-thermal discharge plasmas, it is thought that electron impact dissociative reactions dominate the PFC decomposition processes [1]. High-current electron beams (e-beams) may possibly be employed to generate a nonthermal plasma. E-beams are frequently used in excimer lasers and radiation chemical reactions. An e-beam generated plasma has also been used for the decomposition of carbon tetrachloride [2]. Ions and metastable atoms are efficiently generated using an e-beam. The ion reaction for any PFC will be the dominant decomposition process [3,4], because the energy of secondary electrons produced by the e-beam rapidly decreases to room temperature.

The aim of this study was to determine the decomposition path for PFCs through e-beam generated plasma technology, and to evaluate its theoretical efficiency. We developed a kinetic model of the decomposition of CF_4 in wet argon under e-beam irradiation and determined the optimum concentration of H₂O required for the decomposition process. H₂O is employed as an additive for PFC abatement. Nitrogen and argon are important gases for most applications. The reaction of argon is fairly well understood, compared to the reaction of nitrogen. In non-thermal discharge plasmas, electron impact dissociative reactions, namely dissociative ionization, dissociation, and electron attachment, are the dominant decomposition processes of CF_4 . The reactions are listed in Table 1.

Ions and metastable atoms are more efficiently generated in e-beam generated plasmas compared to discharge plasmas. The secondary electron temperature rapidly decreases to room temperature. Therefore, the dominant decomposition processes of CF_4 are reactions with the ions and metastable atoms of argon; these reactions are listed in Table 2. The reactions of radicals with PFC molecules are less important, because of their relatively small reaction rate coefficients.

The electron attachment reaction of CF_4 , with a crosssection peak of about 7 eV, will occur because secondary electrons have an average energy of about 7 eV for argon [6]. Attachments will be minor events in e-beam generated

Table 1 Electron impact dissociative reaction processes, where the threshold electron energy is lower than 30 eV.

Reaction	$E_{\rm th}~({\rm eV})$	Ref.
Dissociative ionization		
$CF_4 + e^- \rightarrow CF_3^+ + F + 2e^-$	16	[5]
$CF_4 + e^- \rightarrow CF_2^+ + 2F + 2e^-$	21	[5]
$CF_4 + e^- \rightarrow CF^+ + 3F + 2e^-$	26	[5]
Dissociation		
$CF_4 + e^- \rightarrow CF_3 + F + e^-$	13	[5]
$CF_4 + e^- \rightarrow CF_2 + 2F + e^-$	17	[5]
$CF_4 + e^- \rightarrow CF + 3F + e^-$	18	[5]
Electron attachment		
$CF_4 + e^- \rightarrow CF_3 + F^-$	4.65	[5]
$CF_4 + e^- \rightarrow CF_3^- + F$	5.4	[5]

^{2.} Decomposition Mechanisms of CF₄

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Table 2 Ion and radical reaction processes.

Reaction	Rate (cm^3s^{-1})	Ref.
Ion charge exchange		
$CF_4 + Ar^+ \rightarrow CF_3^+ + F + Ar$	7.0×10^{-10}	[7]
$CF_4 + O^+ \rightarrow CF_3^+ + OF$	1.4×10^{-9}	[8,9]
$CF_4 + CO^+ \rightarrow products$	7.6×10^{-10}	[10]
$CF_4 + O_2^+ \rightarrow small reaction$	$< 3 \times 10^{-12}$	[11]
$CF_4 + CO_2^+ \rightarrow small reaction$	~ 0	[10]
$CF_4 + H_2O^+ \rightarrow small reaction$	$< 5 \times 10^{-12}$	[12]
Radical Dissociation		
$CF_4 + Ar^* \rightarrow products$	4×10^{-11}	[13, 14]
$CF_4 + O(^1D) \rightarrow CF_4 + O(^3P)$	$\leq 1.3 \times 10^{-13}$	[15]

plasmas because the energy of secondary electrons rapidly decreases to room temperature. Furthermore, electron impact ionization and dissociation by secondary electrons are also minor events.

The G-values (molecules/100 eV) of argon are as follows [6]:

$$4.89 \text{Ar} \xrightarrow{100 \text{ eV}} 1.08 \text{Ar}^* + 3.82 \text{Ar}^+ + 3.82 \text{e}^-, \qquad (1)$$

where Ar^+ and Ar^* are the argon ion and metastable $Ar({}^{3}P_{0,2})$. Ar^+ and Ar^* have an energy of about 16 and 12 eV, respectively. Both Ar^+ and Ar^* are capable of decomposing CF_4 as shown in Table 2. Hereafter, Ar^+ and Ar^* are called the activated species of argon. Input energy of 70% or more is used to produce the activated species of argon.

An e-beam with input energy density of 1 J/cm^3 generates $\text{Ar}^+ \approx 2.39 \times 10^{17} \text{ cm}^{-3}$ and $\text{Ar}^* \approx 6.75 \times 10^{16} \text{ cm}^{-3}$. The density of the activated species of argon corresponds to 1.25% of the atmospheric-pressure gas density. Therefore, 1.25% of CF₄ in atmospheric-pressure argon gas is decomposed if all of the activated species of argon contribute to the decomposition process. However, many activated species of argon are quenched due to recombination, de-excitation, and radiation, and by the additives H₂O, O₂, H₂, intermediates, and by-products.

The decomposition of CF_4 and the major processes are,

$$\operatorname{Ar}^{+} + \operatorname{CF}_{4} \xrightarrow{k_{1}} \operatorname{CF}_{3}^{+} + F + \operatorname{Ar},$$
 (2)

$$\operatorname{Ar}^{+} + 2\operatorname{Ar} \xrightarrow{k_{2}} \operatorname{Ar}_{2}^{+} + \operatorname{Ar},$$
 (3)

$$Ar^+ + M \longrightarrow Products,$$
 (4)

where $k_1 = 7.0 \times 10^{-10} \text{ cm}^3/\text{s}[7]$, $k_2 = 0.7 \times 10^{-31} \text{ cm}^6/\text{s}$ [16], and k_3 is dependent on the species M, and k_3 is typically 0 to less than $10^{-9} \text{ cm}^3/\text{s}$. M represents the additives H₂O, O₂, and H₂, and the by-products.

$$\operatorname{Ar}_{2}^{+} + e^{-} \longrightarrow \operatorname{Ar}^{*} + \operatorname{Ar},$$
 (5)

$$\operatorname{Ar}_{2}^{+} + M \xrightarrow{k_{5}} \operatorname{Products},$$
 (6)

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where $k_4 = 9.1 \times 10^{-7} \times (T/300 \text{ K})^{-0.61} \text{ cm}^3/\text{s}[17]$ and k_5 is dependent on the species M (k_5 is typically 0 to less than $10^{-9} \text{ cm}^3/\text{s}$).

$$\operatorname{Ar}^* + \operatorname{CF}_4 \xrightarrow{k_6} \operatorname{Products},$$
 (7)

$$\operatorname{Ar}^* + 2\operatorname{Ar} \xrightarrow{k_7} \operatorname{Ar}_2^* + \operatorname{Ar},$$
 (8)

$$\operatorname{Ar}^* + \operatorname{M} \xrightarrow{k_8} \operatorname{Products},$$
 (9)

where $k_6 = 4.0 \times 10^{-11} \text{ cm}^3/\text{s}[14]$, $k_7 = 1.0 \times 10^{-32} \text{ cm}^6/\text{s}$ [18], and k_8 is dependent on the species M (k_8 is typically 0 to less than $10^{-10} \text{ cm}^3/\text{s}$).

$$\operatorname{Ar}_{2}^{*} \xrightarrow{k_{0}} 2\operatorname{Ar} + h\nu,$$
 (10)

$$\operatorname{Ar}_{2}^{*} + M \xrightarrow{k_{10}} \operatorname{Products},$$
 (11)

where $k_9 = 6.0 \times 10^6 \text{ s}^{-1}[19]$ and k_{10} is dependent on the species M (k_{10} is typically 0 to less than $10^{-10} \text{ cm}^3/\text{s}$).

The corresponding rate equations of the CF_4 decomposition are

$$\frac{d[CF_4]}{dt} = -\{k_1[Ar^+] + k_6[Ar^*]\} [CF_4] - \sum_{k} R_d[CF_4], \qquad (12)$$

$$\frac{d[Ar^+]}{dt} = -k_1 [CF_4] [Ar^+]$$

$$\frac{[A\Gamma^{+}]}{dt} = -k_1[CF_4][A\Gamma^{+}] - \left\{k_2[A\Gamma]^2 + \sum k_3[M]\right\}[A\Gamma^{+}], \qquad (13)$$

$$\frac{d[Ar^*]}{dt} = -k_6[CF_4][Ar^*] - \left\{k_7[Ar]^2 + \sum k_8[M]\right\}[Ar^*].$$
(14)

The second term on the right hand side of Eq. (12) corresponds to another decomposition reaction, such as electron impact, which is not effective in e-beam generated plasmas. Therefore, the contribution of this reaction type is not included in our kinetic model. The decomposition rates of CF_4 by Ar^+ and Ar^* are defined by

$$DR_{\rm Ar^+} = \frac{k_1[\rm CF_4]}{k_1[\rm CF_4] + k_2[\rm Ar]^2 + \sum k_3[\rm M]},$$
(15)

and

$$DR_{Ar^*} = \frac{k_6[CF_4]}{k_6[CF_4] + k_7[Ar]^2 + \sum k_8[M]}.$$
 (16)

The reaction diagram for CF₄ at a concentration of 1000 ppm (0.1%) in an e-beam irradiated argon gas at the standard temperature and pressure, and an input energy density of 20 mJ/cm³, is shown in Fig. 1. Here, $DR_{Ar^+} = 0.27$ and $DR_{Ar^+} = 0.13$ were obtained as additives, and the amounts of any by-products were small compared to the CF₄ concentration. As a result, about 25% of the input energy was used in the decomposition of CF₄ and about 2×10^{15} cm⁻³ of CF₄ molecules were decomposed. This value is the ideal limit, and decreases through the reaction of the activated species with additives and by-products.



Fig. 1 Reaction diagram for CF₄ in e-beam irradiated argon gas at standard temperature and pressure (273.15 K and 10^5 Pa). The number density of CF₄ is 2.7×10^{16} cm⁻³. The input energy density is 20 mJ/cm³. The number density of Ar⁺ and electron is 5×10^{15} cm⁻³. The reaction particle and reduction rates are shown on the arrows. Smaller contributions are presented as dotted lines. M represents the H₂O additives and by-products.

The energies of bimolecular-ion Ar_2^+ and dimer Ar_2^* of argon are 14.5 and 11 eV, respectively. The energies are greater than the ionization and dissociation energies of CF₄. However, the decomposition of CF₄ by Ar_2^+ and Ar_2^* has not been confirmed experimentally. The decomposition of CF₄ by Ar_2^+ may be negligible even if Ar_2^+ can operate in the decomposition of CF₄, because Ar_2^+ rapidly dissociates to Ar^* and Ar through dissociative recombination. The decomposition of CF₄ by Ar_2^* may be also negligible even if Ar_2^* can operate in the decomposition of CF₄, because Ar_2^* rapidly dissociates to Ar^* and Ar through radiation emission.

3. The Simulation Model

The implemented numerical method employs a zerodimensional kinetic model of the gas phase, because the ebeam can generate a uniform plasma. Input energy density per pulse in pulse operation is typically 20 mJ/cm³ [20]. The temperature rise is about 50 degrees without radiation loss. In the model, reaction rates at room temperature are used for simplicity.

The reaction of Ar⁺, Ar^{*}, Ar^{*}₂, and Ar^{*}₂ with CF₄ and H₂O and other reactions related to by-products, are included in the model. The quenching reaction of the activated species with the minor intermediate and final products is not included. The reaction of Ar⁺₂ and Ar^{*}₂ with CF₄ is not included in the simulation. The reasons are discussed in the previous section. Typical reactions are listed in Tables 3, 4, 5, 6, and 7. Compositions of hydrocarbon and fluorinated hydrocarbon similar to $C_xH_yF_z$ (x > 1, y > 1, z > 0) are neglected because the composition rate is very small compared to the other reaction rates

Table 3 Ion-molecule reaction processes.

Reaction			Rate (cm ³ /s)	Ref.
$CF_4 + Ar^+$	\rightarrow	$CF_3^+ + F + Ar$	7.0×10^{-10}	[7]
$CF_3 + Ar^+$	\rightarrow	$CF_3^+ + Ar$	1.0×10^{-10}	estimated
$CF_3 + Ar^+$	\rightarrow	$CF_2^+ + F + Ar$	1.0×10^{-10}	estimated
$CF_2 + Ar^+$	\rightarrow	$CF_2^+ + Ar$	1.0×10^{-10}	estimated
$CF_2 + Ar^+$	\rightarrow	$CF^{+} + F + Ar$	1.0×10^{-10}	estimated
$CF + Ar^+$	\rightarrow	$CF^+ + Ar$	1.0×10^{-10}	estimated
$H_2O + Ar^+$	\rightarrow	$H_2O^+ + Ar$	6.8×10^{-10}	[21]
$H_2O + Ar^+$	\rightarrow	$ArH^+ + OH$	3.2×10^{-10}	[21]
$CO + Ar^+$	\rightarrow	$CO^+ + Ar$	4.0×10^{-11}	[21]
$CO_2 + Ar^+$	\rightarrow	$CO_2^+ + Ar$	4.4×10^{-10}	[21]
$O_2 + Ar^+$	\rightarrow	$O_2^+ + Ar$	3.9×10^{-11}	[21]
$O + Ar^+$	\rightarrow	$O^+ + Ar$	6.4×10^{-12}	[22, 23]
$H_2 + Ar^+$	\rightarrow	$ArH^+ + H$	1.25×10^{-9}	[23]
$H_2O + Ar_2^+$	\rightarrow	$H_2O^+ + 2Ar$	1.6×10^{-9}	[21]
$CO + Ar_2^+$	\rightarrow	$CO^+ + 2Ar$	6.1×10^{-10}	[21]
$CO_2 + Ar_2^+$	\rightarrow	$CO_2^+ + 2Ar$	7.7×10^{-10}	[21]
$O_2 + Ar_2^+$	\rightarrow	$O_{2}^{+} + 2Ar$	7.4×10^{-11}	[21]
$H_2 + Ar_2^+$	\rightarrow	$ArH^+ + H + Ar$	3.6×10^{-10}	[24]
$CF_4 + O^+$	\rightarrow	$CF_3^+ + OF$	1.4×10^{-9}	[8,9]
$H + O^+$	\rightarrow	$H^+ + O$	6.80×10^{-10}	[25]
$H_2O + O^+$	\rightarrow	$H_2O^+ + O$	3.2×10^{-9}	[25]
$O + H^+$	\rightarrow	$O^+ + H$	3.75×10^{-10}	[25]
$H_2O + H^+$	\rightarrow	$H_2O^+ + H$	8.2×10^{-9}	[25]
$O_2 + H_2O^+$	\rightarrow	$O_{2}^{+} + H_{2}O$	2.5×10^{-10}	[26]
$H_2 + H_2O^+$	\rightarrow	$H_3O^+ + H$	1.4×10^{-9}	[25]
$H_2O + H_2O^+$	\rightarrow	$H_3O^+ + OH$	1.3×10^{-9}	[27]
$H_2O + ArH^+$	\rightarrow	$H_3O^+ + Ar$	4.5×10^{-9}	[27]

at room temperature.

The ambient total pressure and temperature are 1 atm and 300 K, respectively. The concentration of CF₄ is 1000 ppm for all simulated cases. The concentration of added H₂O is 0 to 3%, near the saturated vapor pressure at T = 300 K. The total gas density is [Ar] + [CF₄] + [H₂O] = 2.45×10^{19} cm⁻³, where [X] is the number density of X and [CF₄] = 2.45×10^{16} cm⁻³.

The input e-beam employs a square pulse, where the pulse width $\tau = 100$ ns. It is assumed that all the input energy is used to excite the argon gas, as represented in by Eq. (1), because the concentrations of CF₄ and H₂O are less than about 1%.

4. Simulation Results

Figure 2 shows the time evolution of the CF₄ density for an input energy density of 20 mJ/cm^3 , when the concentration of H₂O is 1×10^{-5} %, 2.5×10^{-2} %, and 3%. Since the decay time of the activated species of argon is about 100 ns, the decomposition reaction of CF₄ is terminated within about 200 ns. Maximum decomposition is achieved when the concentration of H₂O is 1×10^{-5} %. The number density of the decomposition is $2.0 \times 10^{15} \text{ cm}^{-3}$ and the concentration is about 80 ppm. The number density is in agreement with the estimated value presented in the previous section. However, most of the products of

Reaction			Rate (cm^3/s)	Ref.
$CF_3 + e^-$	\rightarrow	$CF_2 + F^-$	1×10^{-10}	[28]
$CF_2 + e^-$	\rightarrow	$CF + F^-$	1×10^{-10}	[28]
$CF + e^{-}$	\rightarrow	$C + F^{-}$	1×10^{-10}	[28]
$F_2 + e^-$	\rightarrow	$F + F^-$	1.7×10^{-8}	for 298 K [29]
$CF_{3}^{+} + e^{-}$	\rightarrow	$CF_2 + F$	$2.08 \times 10^{-7} \times (T/300 \text{ K})^{-0.48}$	[30, 31]
$CF_{3}^{+} + e^{-}$	\rightarrow	CF + 2F	$0.52 \times 10^{-7} \times (T/300 \mathrm{K})^{-0.48}$	[30, 31]
$CF_{2}^{+} + e^{-}$	\rightarrow	CF + F	$2.63 \times 10^{-7} \times (T/300 \mathrm{K})^{-0.76}$	[30, 31]
$CF_{2}^{2} + e^{-}$	\rightarrow	C + 2F	$1.07 \times 10^{-7} \times (T/300 \mathrm{K})^{-0.76}$	[30, 31]
$CF^{+} + e^{-}$	\rightarrow	C + F	$0.52 \times 10^{-7} \times (T/300 \mathrm{K})^{-0.8}$	[30, 32]
$H_2O^+ + e^-$	\rightarrow	OH + H	$0.86 \times 10^{-7} \times (T/300 \mathrm{K})^{-0.74}$	[30, 33]
$H_2O^+ + e^-$	\rightarrow	$O + H_2$	$0.39 \times 10^{-7} \times (T/300 \text{ K})^{-0.74}$	[30, 33]
$H_2O^+ + e^-$	\rightarrow	O + 2H	$3.05 \times 10^{-7} \times (T/300 \text{ K})^{-0.74}$	[30, 33]
$OH^{+} + e^{-}$	\rightarrow	O + H	$0.375 \times 10^{-7} \times (T/300 \text{ K})^{-0.5}$	[30, 34]
$H_3O^+ + e^-$	\rightarrow	$H_2O + H$	$1.1 \times 10^{-6} \times (T/300 \text{ K})^{-0.5}$	[27]
$CO_{2}^{+} + e^{-}$	\rightarrow	$\overline{CO_2}$	$0.26 \times 10^{-7} \times (T/300 \text{ K})^{-0.8}$	[35]
$CO_{2}^{+} + e^{-}$	\rightarrow	CO + O	$5.65 \times 10^{-7} \times (T/300 \text{ K})^{-0.8}$	[35]
$CO_{2}^{+} + e^{-}$	\rightarrow	$C + O_2$	$0.59 \times 10^{-7} \times (T/300 \text{ K})^{-0.8}$	[35]
$CO^{+} + e^{-}$	\rightarrow	C + 0	1.85×10^{-7}	for 300 K [36]
$O_{2}^{+} + e^{-}$	\rightarrow	20	$1.95 \times 10^{-7} \times (T/300 \text{ K})^{-0.7}$	[37]
$ArH^+ + e^-$	\rightarrow	Ar + H	7×10 ⁻¹⁰	for 5000 K [23]
$Ar_{2}^{+} + e^{-}$	\rightarrow	$Ar^* + Ar$	$9.1 \times 10^{-7} \times (T/300 \text{ K})^{-0.61}$	[17]
$H + F^-$	\rightarrow	$HF + e^{-}$	1.6×10^{-9}	for 296 K [38]
$CF_{3}^{+} + F^{-}$	\rightarrow	$CF_2 + F_2$	8.7×10^{-8}	[28]
$CF_{2}^{+} + F^{-}$	\rightarrow	$CF + F_2$	9.1×10^{-8}	[28]
$CF^{+} + F^{-}$	\rightarrow	CF + F	9.8×10^{-8}	[28]
$O_{2}^{+} + F^{-}$	\rightarrow	$F + O_2$	5×10^{-8}	[39]
$O^{+} + F^{-}$	\rightarrow	$F + O_2$	5×10^{-8}	[39]

Table 4 Electron attachment, dissociative recombination, and negative ion reaction processes. Electron attachment and dissociative recombination reaction depends on the electron temperature; for the processes discussed here, the electron temperature is around room temperature.



Fig. 2 Time evolution of CF₄ densities. The horizontal axis is logarithmic; the solid, dotted, and dashed lines represent H₂O concentrations of 1×10^{-5} %, 2.5×10^{-2} %, and 3%, respectively.

decomposition are reformed to CF₄ because of the small amount of additives. When the concentration of H₂O is 2.5×10^{-2} %, the number density of the decomposition of CF₄ is 1.7×10^{15} cm⁻³. The decomposition efficiency decreases to 15% from the efficiency for an H₂O concentration of 1×10^{-5} %. The carbon and fluorine atoms from the decomposition of CF₄ are efficiently converted to HF, CO₂, and other by-products using oxygen and hydrogen atoms from H₂O as the additives. In contrast, when the concentration of H₂O is 3%, most of the activated species of argon are consumed in the process of decomposing H₂O.

The variation in the density of CF₄ as a function of the H₂O concentration is shown in Fig. 3. The closed circles and triangles represent the minimum and final density of CF₄, respectively. Here, the final density refers to the density when the reformation of CF₄ is complete. For an input energy density of 20 mJ/cm³, the number density of the decomposition of CF₄ is maximum when the H₂O concentration is 2.5×10^{-2} %. As the concentration of H₂O increases from 2.5×10^{-2} %, the efficiency of the decomposition of CF₄ decreases, and most of the activated species of argon are consumed during decomposition of H₂O. As the concentration of H₂O decreases from 2.5×10^{-2} %, the efficiency of the decomposition of CF₄ also decreases, and most decomposition products reform to CF₄.

The change in the concentration of CF_4 for input energy density is shown in Fig. 4. The concentration of H_2O is optimal for each input energy density. The temperature of the gas exceeds 500°C when the input energy density ex-

Reaction			Rate (cm^3/s)	Ref.
$CF_4 + Ar^*$	\rightarrow	$CF_2 + F_2 + Ar$	4.0×10^{-11}	[14]
$CF_3 + Ar^*$	\rightarrow	$CF_2 + F + Ar$	4.0×10^{-11}	estimated
$CF_2 + Ar^*$	\rightarrow	CF + F + Ar	4.0×10^{-11}	estimated
$F_2 + Ar^*$	\rightarrow	Ar + 2F	3.5×10^{-10}	[40]
$F_2 + Ar^*$	\rightarrow	$ArF^* + F$	4.0×10^{-10}	[40]
$H_2O + Ar^*$	\rightarrow	O + 2H + Ar	1.84×10^{-10}	[41-43]
$H_2O + Ar^*$	\rightarrow	OH + H + Ar	2.16×10^{-10}	[41-43]
$O_2 + Ar^*$	\rightarrow	20 + Ar	2.2×10^{-10}	[42]
$CO + Ar^*$	\rightarrow	C + O + Ar	2.7×10^{-11}	[42]
$CO_2 + Ar^*$	\rightarrow	CO + O + Ar	5.6×10^{-10}	[42]
$F_2 + Ar_2^*$	\rightarrow	$Ar_2F^* + F$	2.5×10^{-10}	[44, 45]
$F_2 + Ar_2^{*}$	\rightarrow	$ArF^* + F + Ar$	3.0×10^{-10}	[44]
$F + Ar_2^*$	\rightarrow	$ArF^* + Ar$	3.0×10^{-10}	[44, 45]
$H_2O + Ar_2^*$	\rightarrow	OH + H + 2Ar	1.4×10^{-9}	[46]
$O_2 + Ar_2^*$	\rightarrow	2O + 2Ar	2.6×10^{-10}	[18]
$CO + Ar_2^*$	\rightarrow	CO + 2Ar	1.6×10^{-10}	[18]
$CO_2 + Ar_2^*$	\rightarrow	CO + O + 2Ar	6.8×10^{-10}	[18]
$Ar^* + Ar^*$	\rightarrow	$Ar^+ + Ar + e^-$	5.0×10^{-10}	[47]
$Ar_{2}^{*} + Ar_{2}^{*}$	\rightarrow	$Ar_{2}^{+} + 2Ar + e^{-}$	5.0×10^{-10}	[47]
$Ar^* + Ar_2^*$	\rightarrow	$Ar^+ + 2Ar + e^-$	5.0×10^{-10}	[47]
$ArF^* + (Ar)$	\rightarrow	Ar + F + (Ar)	9.0×10^{-12}	[48, 49]
$Ar_2F^* + (Ar)$	\rightarrow	2Ar + F + (Ar)	2.2×10^{-14}	[50]
$Ar_{2}^{*} + (e^{-})$	\rightarrow	$2Ar + (e^{-})$	1.0×10^{-9}	[51]
$ArF^{*} + (e^{-})$	\rightarrow	$Ar + F + (e^{-})$	1.6×10^{-7}	[52]
$Ar_2F^* + (e^-)$	\rightarrow	$2Ar + F + (e^{-})$	1.0×10^{-7}	[44]
Ar_2^*	\rightarrow	2Ar + hv	$6.0 \times 10^6 \text{ s}^{-1}$	[19]
ArF^*	\rightarrow	$Ar + F + h\nu$	$2.50 \times 10^8 \text{ s}^{-1}$	[45]
Ar_2F^*	\rightarrow	$2Ar + F + h\nu$	$4.3 \times 10^{6} \text{ s}^{-1}$	[50]



Fig. 3 Variations in the density of CF_4 as a function of the concentration of H_2O . Closed circles and triangles represent the minimum and final density of CF_4 , respectively. The time of the final density is 100 ms.

ceeds 200 mJ/cm³ (no cooling is applied). It was assumed for simplicity that the temperature of the gas is unchanged; that is, the same reaction rates are used. A final CF₄ decomposition of 99% is obtained for an input energy density of 1 J/cm³. This input energy density of 1 J/cm³ cor-

Table 6 Radical and molecule reaction processes; gas temperature is 300 K.

Reaction			Rate (cm ³ /s)	Ref.
$CF_3 + O$	\rightarrow	$COF_2 + F$	3.11×10^{-11}	[53]
$CF_2 + O$	\rightarrow	COF + F	1.4×10^{-11}	[54, 55]
$CF_2 + O$	\rightarrow	CO + 2F	4×10^{-12}	[54, 55]
CF + O	\rightarrow	CO + F	3.9×10^{-11}	[56]
COF + O	\rightarrow	$CO_2 + F$	9.3×10^{-11}	[54, 55]
$CF_3 + H$	\rightarrow	$CF_2 + HF$	9.1×10^{-11}	[57]
$CF_2 + H$	\rightarrow	CF + HF	3.9×10^{-11}	[57]
CF + H	\rightarrow	C + HF	1.9×10^{-11}	[57]
$CF_3 + F_2$	\rightarrow	$CF_4 + F$	7.0×10^{-14}	[58]
$CF + F_2$	\rightarrow	$CF_2 + F$	3.9×10^{-12}	[59]
$C + F_2$	\rightarrow	CF + F	2.3×10^{-12}	extrapolated
$H + F_2$	\rightarrow	HF + F	1.5×10^{-12}	[60]
$F + H_2$	\rightarrow	HF + H	2.5×10^{-11}	[61]
$F + H_2O$	\rightarrow	OH + HF	1.4×10^{-11}	[61]
OF + O	\rightarrow	$O_2 + F$	2.7×10^{-11}	[62,63]
OF + H	\rightarrow	HF + O	8.2×10^{-12}	[64]
OF + OF	\rightarrow	$O_2 + F_2$	4.6×10^{-15}	[65]
$COF + CF_2$	\rightarrow	$CF_3 + CO$	3×10^{-13}	[55]
$COF + CF_2$	\rightarrow	$COF_2 + CF$	3×10^{-13}	[55]
$COF + CF_3$	\rightarrow	$CF_4 + CO$	1×10^{-11}	[55]
$COF + CF_3$	\rightarrow	$COF_2 + CF_2$	1×10^{-11}	[55]
COF + COF	\rightarrow	$COF_2 + CO$	1×10^{-11}	[55]
OH + OH	\rightarrow	$H_2O + O$	1.47×10^{-12}	[66]
OH + O	\rightarrow	$O_2 + H$	3.5×10^{-11}	[66]
$C + O_2$	\rightarrow	CO + O	1.6×10^{-11}	[67]
$H_2O_2 + H$	\rightarrow	$H_2O + OH$	4.2×10^{-14}	[68]
$H_2O_2 + H$	\rightarrow	$H_2 + HO_2$	5.15×10^{-15}	[68]
$H_2O_2 + O$	\rightarrow	$OH + HO_2$	1.78×10^{-15}	[66]
$H_2O_2 + OH$	\rightarrow	$H_2O + HO_2$	1.7×10^{-12}	[66]
$HO_2 + H$	\rightarrow	$H_2 + O_2$	5.6×10^{-12}	[66]
$HO_2 + H$	\rightarrow	2OH	7.2×10^{-11}	[66]
$HO_2 + H$	\rightarrow	$H_2O + O$	2.4×10^{-12}	[66]
$HO_2 + O$	\rightarrow	$OH + O_2$	5.7×10^{-11}	[66]
$HO_2 + OH$	\rightarrow	$H_2O + O_2$	1.1×10^{-10}	[66]
$HO_2 + HO_2$	\rightarrow	$H_2O_2 + O_2$	1.63×10^{-12}	[66]

responds to an energy efficiency for CF_4 decomposition of 13 g/kWh.

5. Concluding Remarks

In this paper, we developed a computational method using a kinetic model of CF_4 in wet argon gas under ebeam irradiation. It was found that the activated species Ar^+ and Ar^* decompose CF_4 , and the concentration of H_2O can be optimized for the decomposition of CF_4 . The energy efficiency for CF_4 decomposition was 13 g/kWh for 99% of CF_4 concentration of 1000 ppm in an atmosphericpressure argon gas.

The reaction of the activated species of argon with primary products such as CF_n (n = 1, 2, 3.) are included in the current model. However, the reaction rates are estimated since the actual reaction rates are unknown. Secondary products, such as COF_2 , are not included in the model because the activated species of argon are quenched

Table 7 Three-body reaction rate processes. The pressure and temperature of argon buffer gas were 760 torr and 300 K. The number density of Ar was 2.45×10^{19} cm⁻³. The unit of reaction rate is cm⁶/s when the reaction rates depend quasi-linearly on the buffer gas density. The unit of reaction rate is cm³/s when the reaction rates depend nonlinearly on the buffer gas density.

Reaction			Rate	Ref.
$Ar^{+} + Ar(+Ar)$	\rightarrow	$Ar_{2}^{+}(+Ar)$	0.7×10^{-31}	[16]
$Ar^* + Ar (+Ar)$	\rightarrow	$Ar_{2}^{\tilde{*}}$ (+Ar)	1.0×10^{-32}	[18]
$ArF^{*} + Ar(+Ar)$	\rightarrow	$Ar_2 \tilde{F}^*$ (+Ar)	4.0×10^{-31}	[48, 49]
$Ar^{+} + F^{-} (+Ar)$	\rightarrow	$ArF^{*}(+Ar)$	3.3×10^{-6}	[69]
$Ar_{2}^{+} + F^{-} (+Ar)$	\rightarrow	$ArF^* + Ar(+Ar)$	$2.9 imes 10^{-6}$	[70]
$CF_3 + F(+M)$	\rightarrow	CF_4 (+M)	1.9×10^{-11}	[55]
$CF_2 + F(+M)$	\rightarrow	CF_3 (+M)	1.2×10^{-11}	[55]
CF + F(+M)	\rightarrow	CF_2 (+M)	3.2×10^{-12}	[55]
COF + F(+M)	\rightarrow	COF_2 (+M)	1.3×10^{-11}	[55]
CO + F(+M)	\rightarrow	COF (+M)	1.8×10^{-12}	[55]
F + F(+M)	\rightarrow	F_2 (+M)	6.0×10^{-34}	[71]
OH + OH (+M)	\rightarrow	$H_2O_2(+M)$	2×10^{-31}	analogous to N ₂ [72]
OH + H (+M)	\rightarrow	$H_2O(+M)$	2.6×10^{-31}	[72]
$H + O_2 (+M)$	\rightarrow	HO_2 (+M)	2.0×10^{-32}	[72]
H + H (+M)	\rightarrow	$H_2(+M)$	6.0×10^{-33}	[72]
O + O (+M)	\rightarrow	O ₂ (+M)	1.1×10^{-33}	[73]
CO + O(+M)	\rightarrow	CO ₂ (+M)	9.8×10 ⁻³⁶	[74]



Fig. 4 Concentration of CF_4 at 100 ms as a function of input energy density.

before the secondary products are produced. The assumption applies to an e-beam pulse width less than $1 \mu s$; thus the model can be applied when the e-beam pulse width is less than $1 \mu s$.

The rate of formation of Ar_2^+ from Ar^+ is crucial in the efficient reaction of the decomposition of CF₄. The ion-molecule reaction rate coefficients of three-body ion atom association in argon gas were obtained, and the range was from 0.6 to $5 \times 10^{-31} \text{ cm}^6/\text{s}$ [75]. We use the value $0.7 \times 10^{-31} \text{ cm}^6/\text{s}$ [16] in the simulation. If, however, we use $2.0 \times 10^{-31} \text{ cm}^6/\text{s}$ [76], the maximum number density of decomposed CF₄ for an input energy of 20 mJ/cm³ decreases to $1.3 \times 10^{15} \text{ cm}^{-3}$ from $2.0 \times 10^{15} \text{ cm}^{-3}$.

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